

Assignment 2

- 1.) Assume a control volume, cylindrical in shape with radius r .

For a steady state flow & fixed control volume, we have

$$\oint \rho \vec{v} (\vec{v} \cdot \hat{n}) dS = 0$$

$$\Rightarrow -\rho V \pi a^2 + \rho V_r \cdot 2\pi r h = 0$$

Using $V_r = C_2/r$ $r > a$, we have

$$\Rightarrow C_2 = \frac{Va^2}{2h}$$

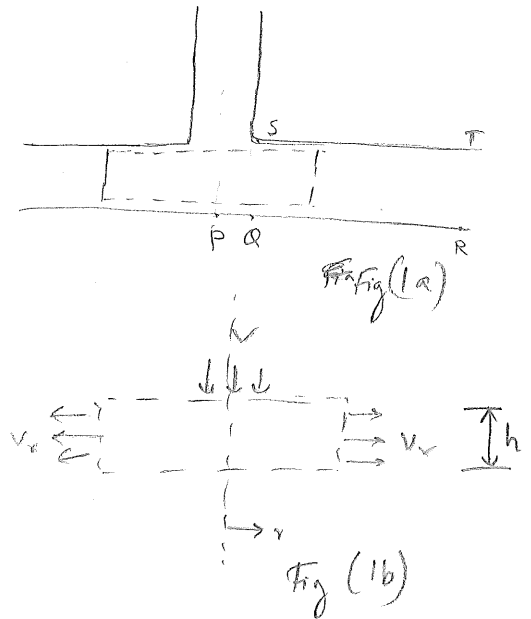
$$\therefore V_r = \frac{Va^2}{2rh} \quad r > a$$

~~At~~ $\therefore V_r = C_1 r$ $r < a$, ~~we balance the~~ we have

$$V_r \Big|_{r=a} = \frac{C_2}{r} \Big|_{r=a} = C_1 r \Big|_{r=a}$$

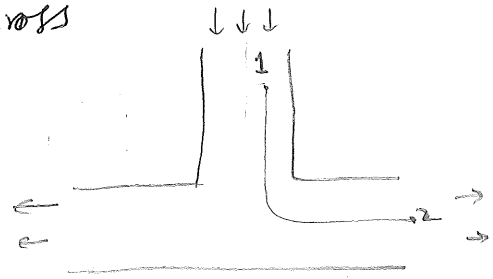
$$\Rightarrow \frac{Va^2}{2ah} = C_1 a \Rightarrow C_1 = \frac{V}{2h}$$

$$\therefore V_r = \begin{cases} \frac{Vr}{2h} & r < a \\ \frac{Va^2}{2rh} & r \geq a \end{cases}$$



1.6) Applying Bernoulli's equation across
1 & 2,

$$P_0 + \frac{1}{2} \rho v^2 = P(r) + \frac{1}{2} \rho v_r^2$$



$$\Rightarrow P(r) - P_0 = \frac{1}{2} \rho v^2 - \frac{1}{2} \rho v_r^2$$

Fig 2

$$= \begin{cases} \frac{1}{2} \rho v^2 \left(1 - \frac{v_r^2}{4v^2} \right) & r < a \\ \frac{1}{2} \rho v^2 \left(1 - \left(\frac{a^2}{2rh} \right)^2 \right) & r \geq a \end{cases}$$

$r < a$

$r \geq a$

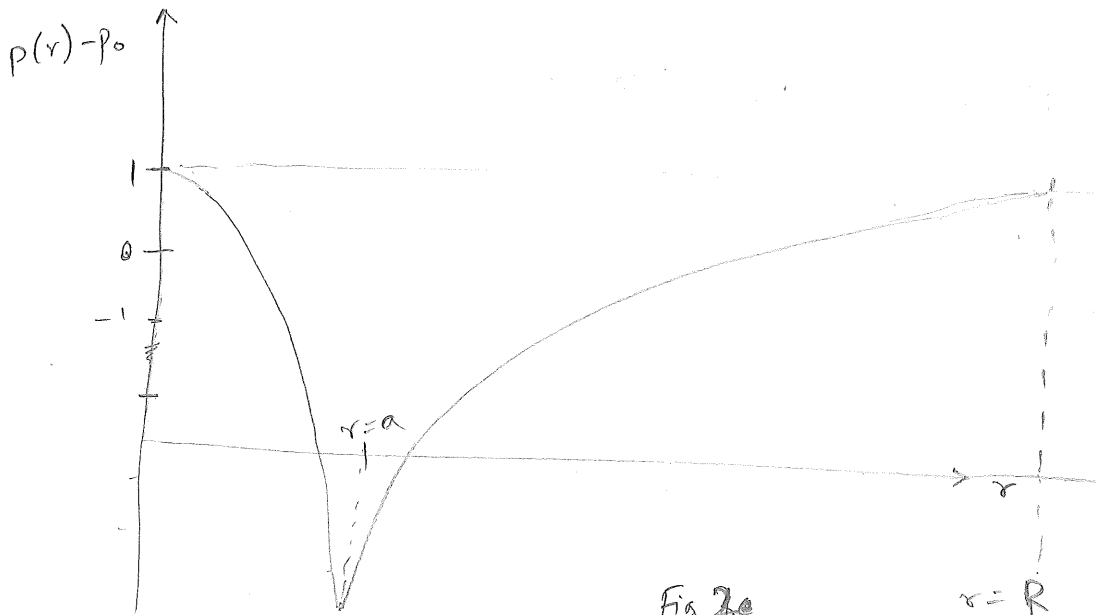


Fig 3a

$$F_p = \int_0^R p(r) \cdot 2\pi r \, dr = \int_0^R (p(r) - p_0) \cdot 2\pi r \, dr$$

$$= \int_0^a \frac{1}{2} \rho v^2 \left(1 - \frac{v_r^2}{4v^2} \right) \cdot 2\pi r \, dr + \int_a^R \frac{1}{2} \rho v^2 \left(1 - \frac{a^4}{4h^2} \cdot \frac{1}{r^2} \right) \cdot 2\pi r \, dr$$

$$= \frac{1}{2} \rho v^2 \cdot \pi R^2 - \frac{1}{2} \rho v^2 \int_0^a \frac{v_r^2}{2} \, dr$$

$$= \frac{1}{2} \rho v^2 \cdot \pi R^2 - \frac{1}{2} \rho v^2 \cdot 2\pi \left[\int_0^a \frac{r^2}{4h^2} \cdot r dr + \int_a^R \frac{a^4}{4h^2} \frac{1}{r^2} r dr \right]$$

$$= \frac{1}{2} \rho v^2 \cdot \pi R^2 - \frac{1}{2} \rho v^2 \cdot 2\pi \left[\frac{a^4}{16h^2} + \frac{a^4}{4h^2} \ln \frac{R}{a} \right]$$

$$= \frac{1}{2} \pi \rho v^2 \left[R^2 - \frac{a^4}{8h^2} \right] - \frac{1}{2} \rho v^2 \cdot 2\pi \frac{a^4}{4h^2} \ln \frac{R}{a}$$

$$= \frac{1}{2} \pi \rho v^2 \left[R^2 - \frac{a^4}{8h^2} \right] + \rho v^2 \pi \frac{a^4}{4h^2} \ln \frac{a}{R}$$

this force can be negative when $\frac{a^2}{h} \ll R$

$\frac{a^2}{h} \gg R$ & $a \ll R$.

Using $a = 0.01 \text{ m}$, $R = 0.05 \text{ m}$, $h = 10^{-3} \text{ m}$, $m = 0.01 \text{ kg}$,
we get velocity as:

$$v = 1.73 \text{ m/s}$$

d) Using the control volume shown in Fig 1(b), we we apply the Reynold's transport theorem. Here the parameter 'h' is ~~not~~ a function of time.

$$\frac{d}{dt} \int_{V_t} \rho dV = \int_{V_t} \frac{d\rho}{dt} dV + \int \rho \vec{v} \cdot \hat{n} ds$$

$$\Rightarrow \frac{d}{dt} (\rho \pi \frac{a^2}{2} h) = -\rho v \cdot \pi a^2 + \rho v r \cdot 2\pi r h$$

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$$\Rightarrow \rho r^2 \frac{dh}{dt} = \rho a^2 v - 2\rho r h v_r$$

$$\Rightarrow v_r = \frac{-r h'}{2h} + \frac{a^2 v}{2hr}, \quad r > a$$

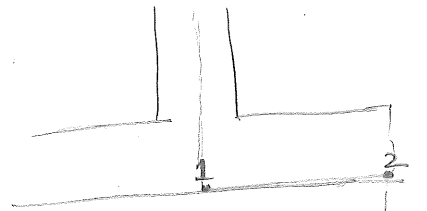
also, considering $v_r = c_1(h, h) r$ $r < a$, we get

$$c_1(h, h) r \Big|_{r=a} = -\frac{a h'}{2h} + \frac{a v}{2h}$$

$$\Rightarrow c_1 = \frac{v}{2h} - \frac{h'}{2h}$$

$$\therefore v_r = \begin{cases} \left(\frac{v-h'}{2h}\right) r & r < a \\ -\frac{r h'}{2h} + \frac{a^2 v}{2hr} & r \geq a \end{cases}$$

Applying Bernoulli's theorem over streamline in Fig 2,



$$\int_1^2 \frac{dv}{dt} ds + \left[\frac{v^2}{2} + \frac{p}{\rho} \right]_1^2 = 0$$

$$\Rightarrow \int_1^2 \frac{dv}{dt} ds = \int_0^a \frac{-h''}{2h} r \cdot dr + \int_a^R \left[-\frac{r h'}{2h} - \frac{h'}{h^2} \left(\frac{a^2 v - r^2 h'}{2r} \right) \right] r dr$$

$$= p_1 + \frac{v_1^2}{2} - p_2 - \frac{v_2^2}{2}$$

$$= p_1 - p_2 - \left(\frac{a^2 v - r^2 h'}{2h} \right)^2$$

2.) a) Boundary conditions

~~$$\vec{v} \Big|_{x \rightarrow -\infty} = v_x \hat{i} + 0 \hat{j}$$~~

$$\vec{v} \Big|_{x \rightarrow -\infty} = U \hat{i} + 0 \hat{j}$$

$$\Delta \quad \vec{v} \cdot \hat{n} \Big|_{r=R} = 0$$

~~$$\Rightarrow \frac{\partial \psi}{\partial y} \Big|_{x \rightarrow -\infty} = U$$~~

$$\& \quad \frac{1}{r} \frac{\partial \psi}{\partial \theta} \Big|_{r=R} = 0$$

b) $\psi(r, \theta) = r^\alpha \sin \theta.$

$$\nabla^2 \psi = 0$$

$$\Rightarrow \frac{\partial^2 \psi}{\partial r^2} + \frac{1}{r} \frac{\partial \psi}{\partial r} + \frac{1}{r^2} \frac{\partial^2 \psi}{\partial \theta^2} = 0$$

$$\Rightarrow \alpha(\alpha-1) r^{\alpha-2} \sin \theta + \alpha r^{\alpha-2} \sin \theta - r^{\alpha-2} \sin \theta = 0$$

$\Rightarrow \therefore$ this must be true for any r & θ ,

$$\Rightarrow \alpha(\alpha-1) + \alpha - 1 = 0$$

$$\Rightarrow \alpha = 1, -1$$

$$\therefore \psi = A r \sin \theta + \frac{B}{r} \sin \theta = A y + \frac{B y}{x^2 + y^2}$$

Applying boundary conditions,

$$\Rightarrow \frac{\partial \psi}{\partial y} \Big|_{x \rightarrow -\infty} = A = U$$

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$$\& \quad \frac{1}{r} \frac{\partial \psi}{\partial \theta} \Big|_R = \left[A \cos \theta + \frac{B}{r^2} \cos \theta \right]_{r=R} = 0$$

$$\Rightarrow A + \frac{B}{R^2} = 0$$

$$\Rightarrow B = -AR^2 = -UR^2$$

$$\therefore \psi = U r \sin \theta - U \frac{R^2}{r} \sin \theta$$

$$= UR \sin \theta \left(\frac{r}{R} - \frac{R}{r} \right)$$

$$V_\theta = -\frac{\partial \psi}{\partial r}$$

$$= -UR \sin \theta \left(\frac{1}{R} + \frac{R}{r^2} \right) = U \sin \theta \left(1 + \frac{R^2}{r^2} \right)$$

& Compute pressure on cylinder using Bernoulli's theorem,

$$P_0 + \frac{1}{2} \rho U^2 = P(\theta) + \frac{1}{2} \rho U^2 \sin^2 \theta \left(1 + \frac{R^2}{R^2} \right)$$

$$\Rightarrow P(\theta) = P_0 + \frac{1}{2} \rho U^2 [1 - 2 \sin^2 \theta]$$

The net force on cylinder :

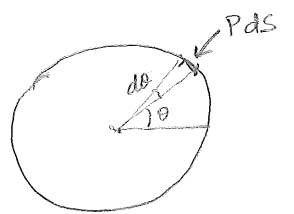
$$dF_x = -P ds \cos \theta, \quad dF_y = -P ds \sin \theta$$

where $ds = r d\theta$, $P = P(\theta)$

$$F_x = \int dF_x = \int_0^{2\pi} \left[P_0 + \frac{1}{2} \rho U^2 (1 - 2 \sin^2 \theta) \right] \cos \theta d\theta$$

$$= \int_0^{2\pi} (P_0 + \frac{1}{2} \rho U^2) \cos \theta d\theta - \frac{1}{2} \rho U^2 \int_0^{2\pi} 2 \sin^2 \theta \cos \theta d\theta$$

$$= 0$$



1/16y, $F_y = \int dF_y = 0$. There is no net force because the flow is inviscid. Hence, the drag force is zero.